In the claims:

Please amend the claims as shown below:

1. (Currently amended) A method for continuous alkali oxygen delignification of digested cellulose pulp and of cellulose pulp that has been washed after digestion, comprising: ~~which~~storing pulp ~~is stored~~ in a storage tower or pulp chute at essentially atmospheric pressure, ~~and that~~ maintaining~~s~~ a medium consistency of the pulp in a~~the~~ range of 8-18%, ~~and that~~ maintaining~~s~~ the cellulose pulp to be delignified at a kappa value of at least 15 units, ~~preferably a kappa exceeding 20 units, where~~ the oxygen delignification taking~~takes~~ place in a reactor system with several oxygen reactors with a predetermined retention time of the cellulose pulp in the reactor system, ~~where~~ adding alkali ~~is added~~ to the cellulose pulp in order to obtain an initial pH exceeding 9.0 and adding~~where~~ oxygen ~~is added~~ to the cellulose pulp at an amount of 5-50 kg per ton~~ne~~ of pulp at a position before a first oxygen reactor in the reactor system, providing~~and where~~ the pulp with~~has~~ a predetermined total retention time of greater than 45 minutes in the reactor system, ~~characterised in that,~~ in association with an~~the~~ addition of ~~the necessary chemicals~~ chemicals and an initial mixing-in operation, placing the cellulose pulp ~~is placed~~ under pressure at an initial pressure of greater than 15.0 bar, subjecting~~after which~~ the pulp ~~is subject~~ to more than one remixing position where a~~the~~ final pressure after a~~the~~ final remixing position is at least 13 bar, subjecting the pulp to~~and with~~ a minimum retention time in a high~~in this first high~~ pressure section of at least 3-10 minutes, reducing~~after which~~ the pressure of the pulp ~~is reduced~~ to a pressure that lies under 10-12 bar, heating the pulp with

~~and is heated by~~ steam such that a~~the~~ temperature of the pulp is raised by at least 5 °C by the addition of steam, and leading~~followed by~~ the heated pulp ~~being led~~ to a reactor system in a low pressure section with a retention time that exceeds the retention time in the high pressure section.

2. (Currently amended) The method according to claim 1, ~~characterised in that~~ wherein oxygen, ~~preferably the major part of the oxygen added for the oxygen stage,~~ is added to the cellulose pulp immediately after the initial pressure of more than 15 bar has been established.

3. (Currently amended) The method according to claim 2, ~~characterised in that~~ wherein the remixing positions are constituted by fluidising mixers, either in a~~the~~ form of a fluidising pump, a fluidising restriction, a fluidising mixer or a restriction in a~~the~~ flow that results in a fall in pressure of less than 1 bar.

4. (Currently amended) The method according to claim 3, ~~characterised in that~~wherein a first high pressure reactor is located after the initial mixing-in operation, in which reactor the cellulose pulp is given a first retention time of t_1, and in that a high pressure reactor follows after the remixing positions in the high pressure section after each one of the remixing positions.

5. (Currently amended) The method according to claim 4, ~~characterised in that~~ wherein the reactors in the high pressure section are dimensioned such that the cellulose pulp is given successively longer retention times, such that when~~if~~ the number of reactors is X, the retention times are $t_1 - t_x$ for each relevant reactor $R_1 - R_x$, where $t_1 < t_2 < .. t_x$.

6. (Currently amended) The method according to claim 5, ~~characterised in that~~wherein the retention times t_1 - t_X in the reactors R_1 - R_X in the high pressure section are expressed as

t_{min} = 1 minute for t_1, after which (t_x=2 * t_{x-1}) and T_{max}= X *10 minutes;

(t_1=1-10 min., t_2=2-20 min.; t_3=4-30 min.; t_4=8-40 min. ~~etc.~~),

where $t_X < t_{X+1}$.

7. (Currently amended) The method according to ~~any one of the preceding claims, characterised in that~~ claim 1 wherein a stirrer is present in at least one high pressure reactor, which stirrer acts in a~~the~~ principal part ~~(greater than 50%)~~ of a~~the~~ reactor volume, either in a~~the~~ form of a mechanical stirrer (S) or hydrodynamic stirrers that at least circulate free fluid in the reactor.

8. (Currently amended) The method according to ~~any one of the preceding claims, characterised in that~~ claim 1 wherein at least one of the oxygen and ~~and~~ alkali additions are ~~can be~~ added to the cellulose pulp in association with the remixing positions in the high pressure section at an amount that is lower than the amount that is added at the initial mixing-in operation, and ~~in that~~ at least one of the oxygen and alkali additions are ~~can~~ ~~be~~ added batch-wise at a~~the~~ beginning of the low pressure section.

9. (Currently amended) The method according to ~~any one of the preceding claims, characterised in that~~ claim 1 wherein the cellulose pulp is dewatered before the oxygen delignification to a higher consistency and ~~in that it~~ the cellulose pulp is re-diluted before the oxygen delignification to a medium consistency with pure filtrate

that has ~~preferably~~ been previously oxidi~~z~~sed, and in that alkali in a~~the~~ form of oxidi~~z~~sed white liquor is used in the oxygen delignification.